

The following pages of data and physical properties are provided as references in the use and application of Spiral pipe and fittings.

The complexity of air system design engineering has changed dramatically since the 1950's even though the basic formulas have still remained the same. There have been significant additional theories added with new extremely complex and systematic formulas needed to satisfy these computations and provide for further enhancement of the overall systems of today. We have tried to give you the basic information needed for both methods. The old rule of thumb method seems to be the simplest method for smaller and moderate jobs. For complex jobs, we still recommend a certified engineer.

The new method of static loss calculations is far too complex for the average Joe. Therefore, we have given you the quick reference chart approach to simplify and speed up the process.

Basic Definitions

The following are used to describe airflow and will be used extensively in this catalog. Standard air is defined at standard atmospheric pressure (14.7 psia), room temperature (70° F) and zero water content; its value is normally taken to be 0.075 lbs/ft³.

The volumetric flow rate, many times referred to as "volumes," is defined as the volume or quantity of air that passes a given location per unit of time, i.e. (cfm). It is related to the average velocity and the flow cross-section area in ft² by the equation

$$Q=VA$$

where Q = volumetric flow rate or cfm,
V= average velocity or fpm, and
A= cross-sectional area in ft².

Given any two of these three quantities, the third can readily be determined as follows:

$$Q=VA \text{ or } V=Q/A \text{ or } A=Q/V$$

There are three different but mathematically related pressures associated with a moving air stream. Static pressure (SP) is defined as the pressure in the duct that tends to burst or collapse the duct and is expressed in inches of water gage ("wg).

Velocity pressure (VP) is defined as that pressure required to accelerate air from zero velocity to some velocity (V) and is proportional to the kinetic energy of the air stream. Using standard air, the relationship between V and VP is given by

$$V = 4005 \sqrt{VP} \text{ or } VP = \left(\frac{V}{4005} \right)^2$$

VP will only be exerted in the direction of airflow and is always positive.

Total pressure (TP) is defined as the algebraic sum of the static and velocity pressures or TP=SP+VP. Total pressure can be positive or negative with respect to atmospheric pressure and is a measure of energy content of the air stream, always dropping as the flow proceeds downstream through a duct. The only place it will rise is across the fan. Total pressure can be measured with a pitot tube pointing directly upstream and connected to a manometer.

Principles of air flow

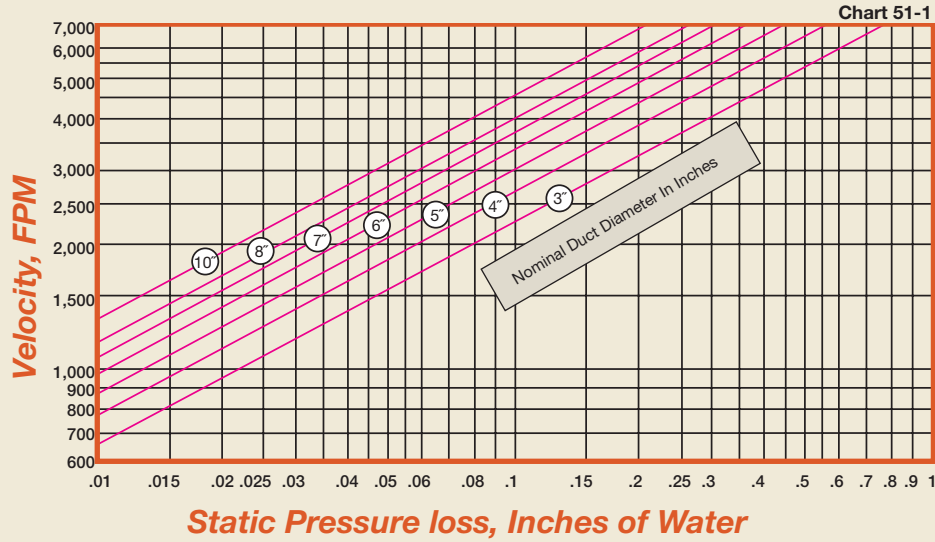
Two basic principles of fluid mechanics govern the flow of air in industrial ventilation systems: conservation of mass and conservation of energy. These are essentially bookkeeping laws which state that all mass and all energy must be completely accounted for and it is important to know what simplifying assumptions are included in the principles discussed below:

1. Heat transfer effects are neglected. However, if the temperature inside the duct is significantly different than the air temperature surrounding the duct, heat transfer will occur. This will lead to changes in the duct air temperature and hence in the volumetric flow rate.
2. Compressibility effects are neglected. However, if the overall pressure drop from the start of the system to the fan is greater than about 20 "wg, then the density needs to be accounted for.
3. The air is assumed to be dry. Water vapor in the air stream will lower the air density, and correction for this effect, if present, should be made.
4. The weight and volume of the contaminant in the air stream is ignored. This is permissible for the contaminant concentrations in typical exhaust ventilation systems. For high concentrations of solids or significant amounts of some gases other than air, corrections for this effect should be included. **(Continued on page 54)**

Engineering Data

Static Pressure (SP) Loss for 90° and 45° Die-Formed Elbows

Static Pressure Loss of Die-Formed 90° Elbows



Static Pressure Loss of Die-Formed 45° Elbows

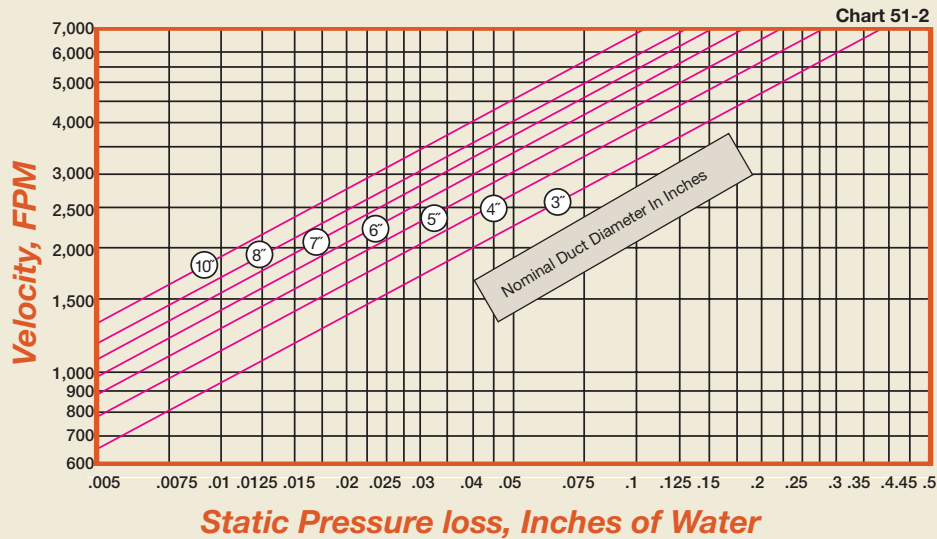


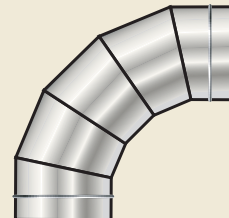
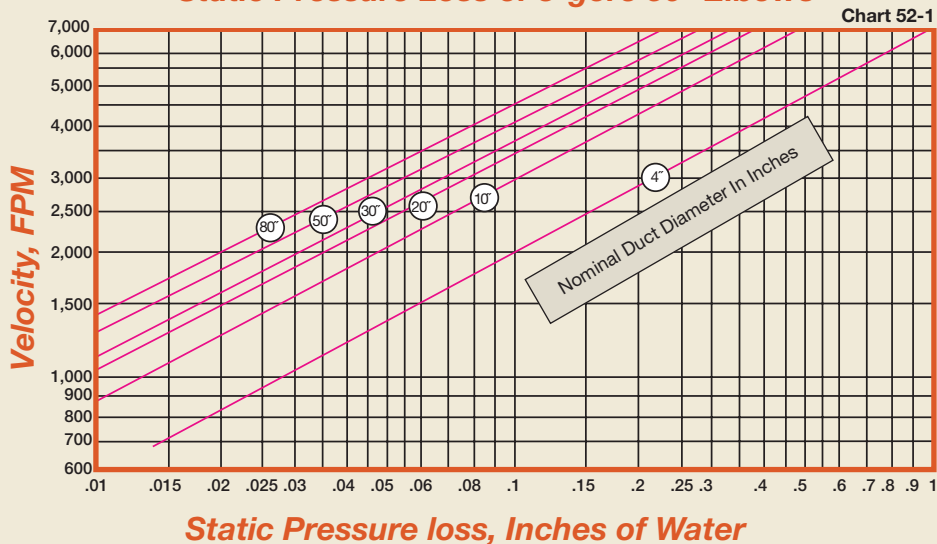
Table 51-1: Duct Pressure Loss Results for Stamped (1.5CLR) Elbows @ 4000 ft/min with .999 (VP)

Size	3"	4"	5"	6"	7"	8"	9"	10"	12"	14"	Elbow Loss Factor
Straight Duct Loss (inches Water):	10.15	7.04	5.31	4.22	3.49	2.95	2.55	2.24	1.79	1.48	
Total Duct Loss (wg) 90° Stamped	10.30	7.18	5.46	4.37	3.63	3.01	2.70	2.39	1.94	1.63	0.15
Total Duct Loss (wg) 45° Stamped	10.22	7.11	5.38	4.30	3.56	3.14	2.62	2.32	1.86	1.56	0.075
Flow Rate: SCFM	192.5	342.3	534.8	770.2	1068	1396	1732.5	2140	3080	4194	

Based per 100 feet duct length • viscosity (cP).018 • Inlet pressure (psig) 0 • Temp (F) 70° • Galvanized metal roughness (ft) .0005 • Flow region Turbulent, 4000fpm • friction factor 0.02 • velocity pressure .999

Static Pressure (SP) Loss for 90° and 45°, 5-Gore and 3-Gore Elbows

Static Pressure Loss of 5-gore 90° Elbows



Static Pressure Loss of 3-gore 45° Elbows

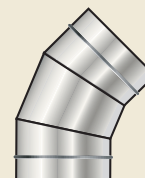
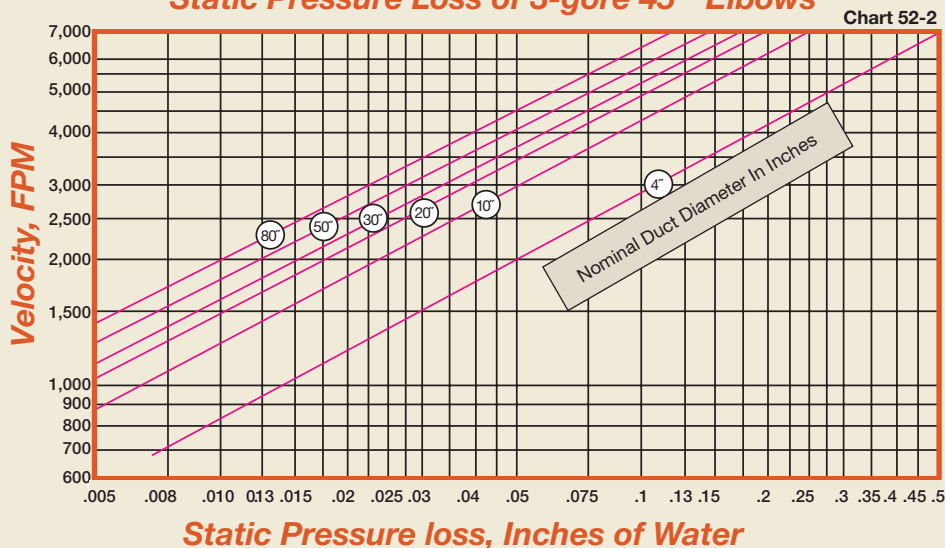


Table 52-1: Duct Pressure Loss Results for Gored (1.5CLR) Elbows @ 4000 ft/min with .999 (VP)

Size	3"	4"	5"	6"	7"	8"	9"	10"	12"	14"	Elbow Loss Factor
Straight Duct Loss (inches Water):	10.15	7.04	5.31	4.22	3.49	2.95	2.55	2.24	1.79	1.48	
Total Duct Loss ("wg) 90° 5 Gore	10.39	7.25	5.55	4.46	3.72	3.19	2.79	2.48	2.03	1.72	0.24
Total Duct Loss ("wg) 45° 3 Gore	10.32	7.21	5.48	4.39	3.65	3.21	2.72	2.41	1.96	1.65	0.17
Flow Rate: SCFM	192.5	342.3	534.8	770.2	1068	1396	1732	2140	3080	4194	

Based per 100 feet duct length • viscosity (cP).018 • Inlet pressure (psig) 0 • Temp (F) 70° • Galvanized metal roughness (ft) .0005 • Flow region Turbulent, 4000fpm • friction factor 0.02 • velocity pressure .999

Engineering Data

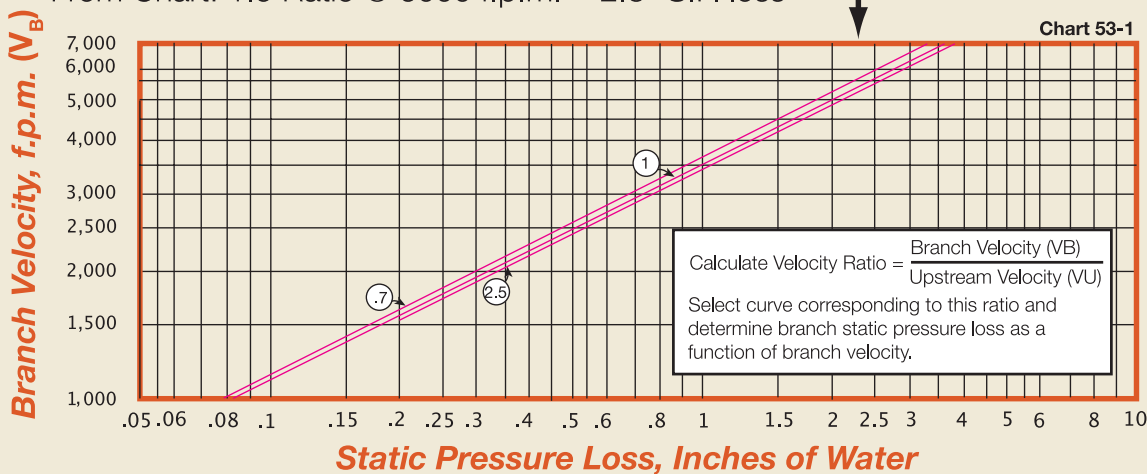
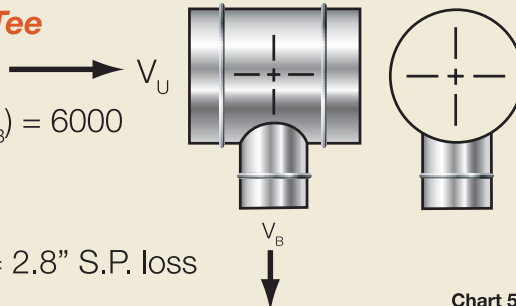
Static Pressure (SP) Loss in 90° Tees & Conical Tees

Static Pressure loss in 90° Tee

Example: Main (V_U) = 4000, Branch (V_B) = 6000

$$\text{Velocity Ratio} = \frac{V_B}{V_U} = \frac{6000}{4000} = 1.5$$

From Chart: 1.5 Ratio @ 6000 f.p.m. \approx 2.8" S.P. loss

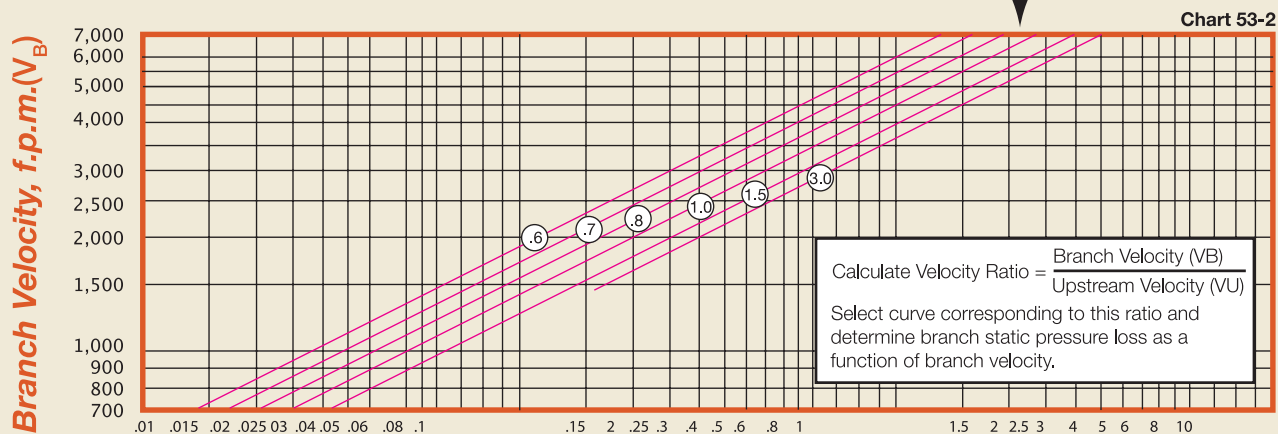
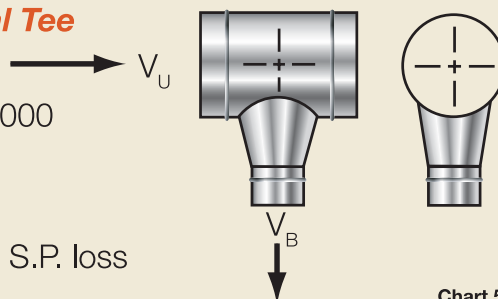


Static Pressure loss in 90° Conical Tee

Example: Main (V_U) = 4000, Branch (V_B) = 6000

$$\text{Velocity Ratio} = \frac{V_B}{V_U} = \frac{6000}{4000} = 1.5$$

From Chart: 1.5 Ratio @ 6000 f.p.m. \approx 2.3" S.P. loss



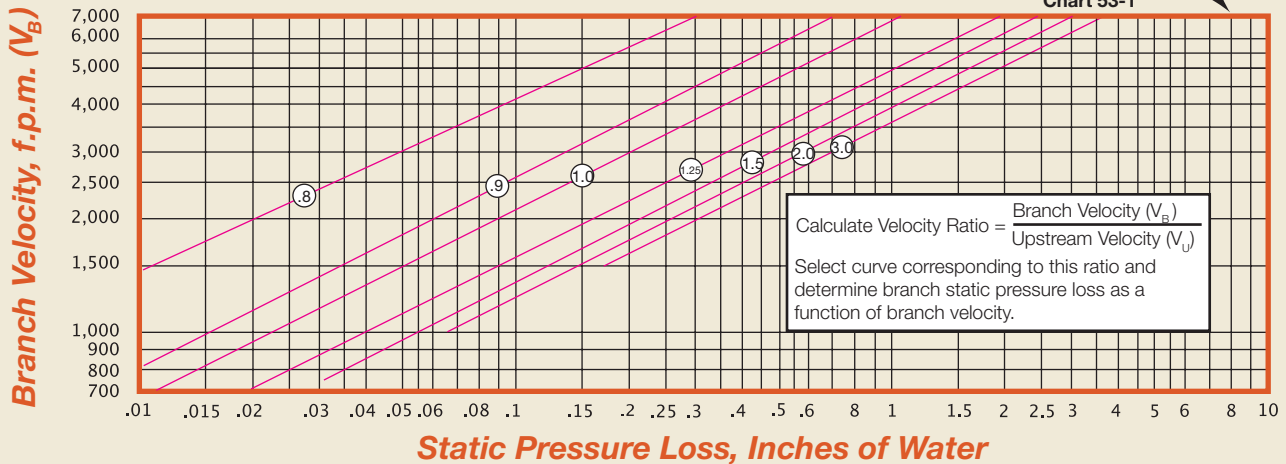
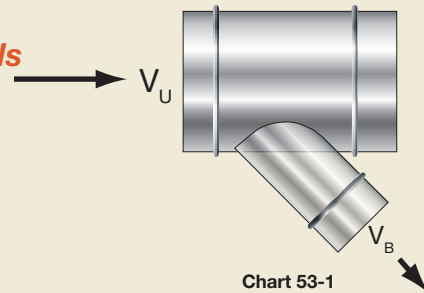
Static Pressure (SP) Loss in 45° Laterals & Branch Entry Loss

Static Pressure loss in 45° Laterals

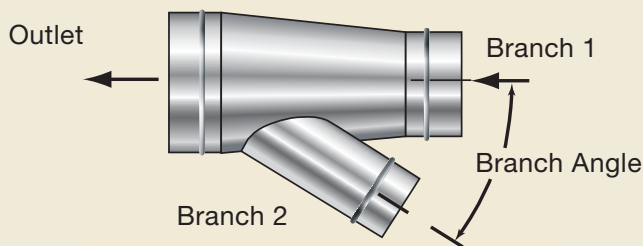
Example: Main (V_U) = 4000, Branch (V_B) = 6000

$$\text{Velocity Ratio} = \frac{V_B}{V_U} = \frac{6000}{4000} = 1.5$$

From Chart: 1.5 Ratio @ 6000 f.p.m. \approx 1.9" S.P. loss



Branch Entries



Note that branch entry loss is assumed to occur in the branch for calculations. Enlargement regain should not be included in branch entry enlargements. Any losses due to acceleration of combined flow should be added to the calculations in the outlet pipe.

(Continued from page 50)

Conservation of mass requires that the net change of mass flow rate must be zero. If the effects discussed on page 51 are negligible, then the density will be constant and the net change of volumetric flow rate (Q) must be zero. Therefore, the flow rate that enters a hood must be the same as the flow rate that passes through the duct leading from the hood. At a branch entry, the sum of the two flow rates that enter the fitting must be equivalent to the total leaving the fitting.

Table 54-1: Equivalent Resistance in Feet of Straight Duct

Size	30°	45°	Size	30°	45°
3"	3	4	20"	18	28
4"	4	6	22"	20	31
5"	5	7	24"	22	34
6"	6	9	26"	24	37
7"	6	10	28"	26	40
8"	7	11	30"	28	43
9"	8	13	32"	29	45
10"	9	14	34"	31	48
12"	11	17	36"	33	51
14"	13	20	38"	35	54
16"	15	23	40"	37	57
18"	17	26	42"	39	60

Equivalent Resistance & Friction Loss Quick Reference Charts

Table 55-1: Elbow Equivalent Resistance In Feet Of Straight Pipe By Center Line Radius (CLR)

Size	1.5 CLR				2.0 CLR				2.5 CLR			
	90° Elbow	60° Elbow	45° Elbow	30° Elbow	90° Elbow	60° Elbow	45° Elbow	30° Elbow	90° Elbow	60° Elbow	45° Elbow	30° Elbow
3"	5	3	3	2	3	2	2	1	3	2	2	1
4"	6	4	3	2	4	3	2	1	4	3	2	1
5"	9	6	5	3	6	4	3	2	5	3	3	2
6"	12	8	6	4	7	5	4	2	6	4	3	2
8"	13	9	7	4	9	6	5	3	7	5	4	2
10"	15	10	8	5	10	7	5	3	8	5	4	3
12"	20	13	10	7	14	9	7	5	11	7	6	4
14"	25	17	13	8	17	11	9	6	14	9	7	5
16"	30	20	15	10	21	14	11	7	17	11	9	6
18"	36	24	18	12	24	16	12	8	20	13	10	7
20"	41	28	21	14	28	19	14	9	23	15	12	8
22"	46	31	23	15	32	21	16	11	26	17	13	9
24"	57	38	29	19	40	27	20	13	32	21	16	11
30"	74	50	37	24	51	34	26	17	41	28	21	14
36"	93	62	47	31	64	43	32	21	52	35	26	17
40"	105	70	53	35	72	48	36	24	59	40	30	20
48"	130	87	65	43	89	60	45	29	73	49	37	24

Losses in Elbows and Fittings. When an air stream undergoes change of either direction or velocity, a dynamic loss occurs. Unlike friction losses in straight duct, fitting losses are due to internal turbulence rather than skin friction. Hence roughness of material has but slight effect over a wide range of moderately smooth materials. Fitting losses can be expressed as equivalent length of straight duct; or as a fraction of velocity pressure; or directly in inches of water gage ("wg).

Table 55-2: Friction Loss In Inches Of Water ("WG) Per 100 Feet Of Spiral Pipe

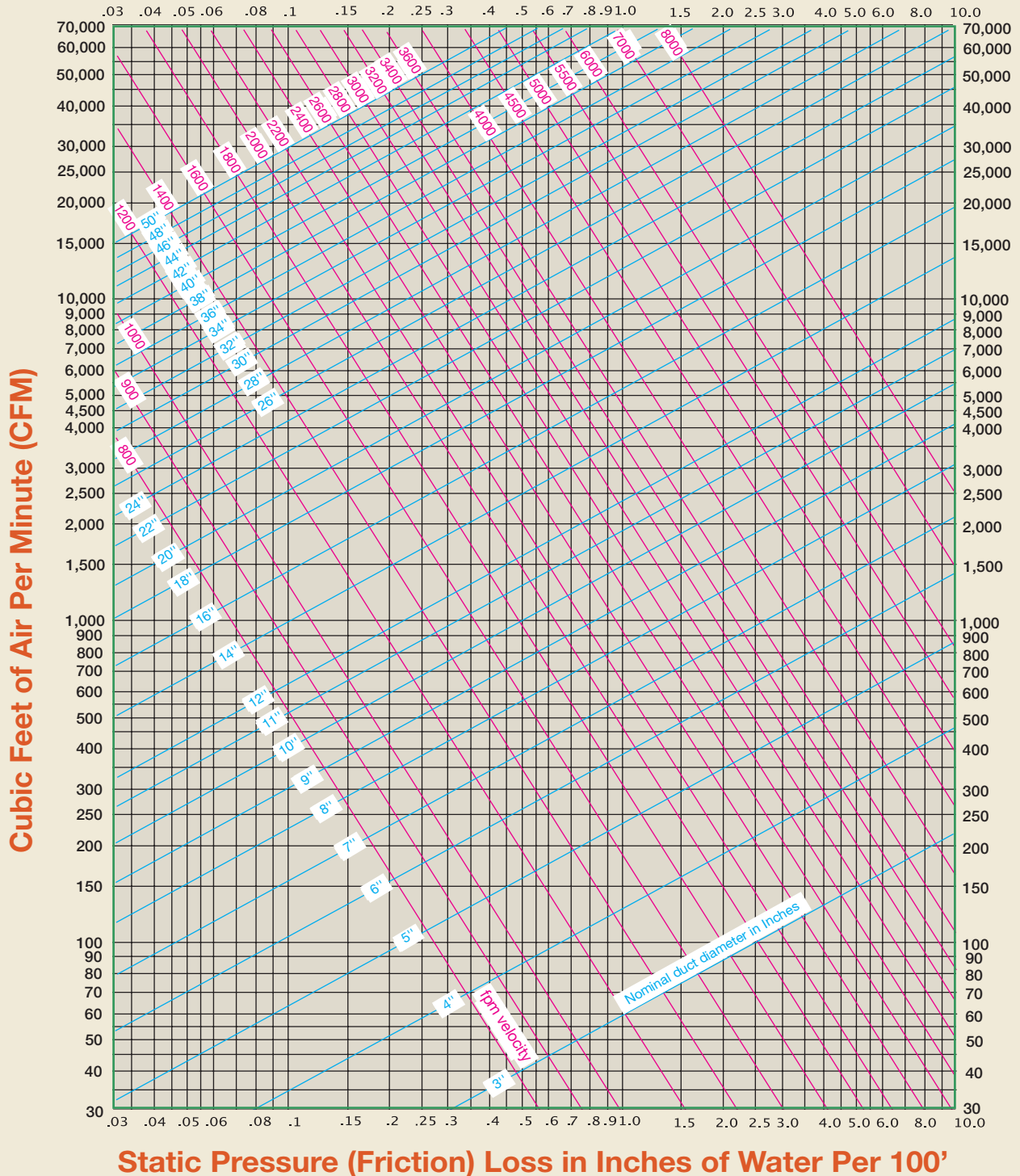
Duct Dia.	Velocity FPM				Duct Dia.	Velocity FPM				Duct Dia.	Velocity FPM			
	3500	4000	4500	5000		3500	4000	4500	5000		3500	4000	4500	5000
3"	7.75	9.99	12.50	15.27	17"	0.93	1.20	1.51	1.84	44"	0.29	0.38	0.47	0.58
4"	5.46	7.03	8.80	10.75	18"	0.87	1.12	1.40	1.72	46"	0.28	0.36	0.45	0.55
5"	4.16	5.36	6.70	8.19	20"	0.77	0.99	1.23	1.51	48"	0.26	0.34	0.42	0.52
6"	3.33	4.29	5.36	6.55	22"	0.68	0.88	1.01	1.34	50"	0.25	0.32	0.40	0.49
7"	2.76	3.55	4.44	5.43	24"	0.61	0.79	0.99	1.21	52"	0.24	0.31	0.38	0.47
8"	2.34	3.02	3.78	4.61	26"	0.56	0.72	0.90	1.01	54"	0.23	0.29	0.37	0.45
9"	2.03	2.62	3.27	4.00	28"	0.51	0.65	0.82	1.00	56"	0.22	0.28	0.35	0.43
10"	1.78	2.30	2.88	3.51	30"	0.47	0.60	0.75	0.92	58"	0.21	0.27	0.34	0.41
11"	1.59	2.05	2.56	3.13	32"	0.43	0.56	0.70	0.85	60"	0.20	0.26	0.32	0.39
12"	1.43	1.84	2.30	2.81	34"	0.40	0.52	0.65	0.79					
13"	1.30	1.67	2.09	2.55	36"	0.37	0.48	0.60	0.74					
14"	1.18	1.53	1.91	2.33	38"	0.35	0.45	0.56	0.69					
15"	1.09	1.40	1.75	2.14	40"	0.33	0.42	0.53	0.65					
16"	1.01	1.30	1.62	1.98	42"	0.31	0.40	0.50	0.61					

$$h_f = 2.74 \frac{(V/1000)^{1.9}}{D^{1.22}}$$

h_f = Friction losses in a duct, "wg.
 V = Duct Velocity, fpm
 D = Duct Diameter, Inches

This equation gives the friction losses, expressed as "wg per 100 feet of pipe, for standard air of 0.075 lbm/ft³ density flowing through average, clean, round galvanized pipe having approximately 40 slip joints per 100 feet ($k = 0.0005$ ft.).

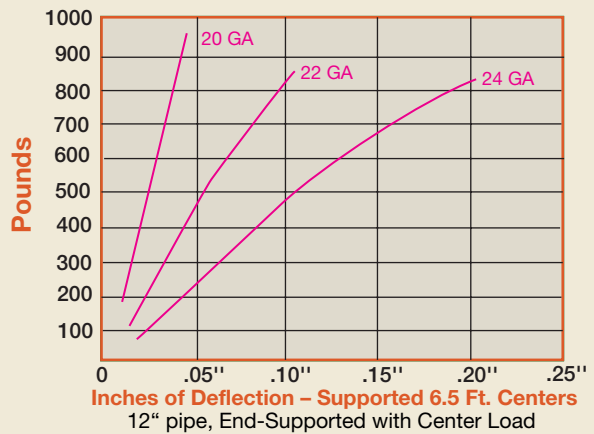
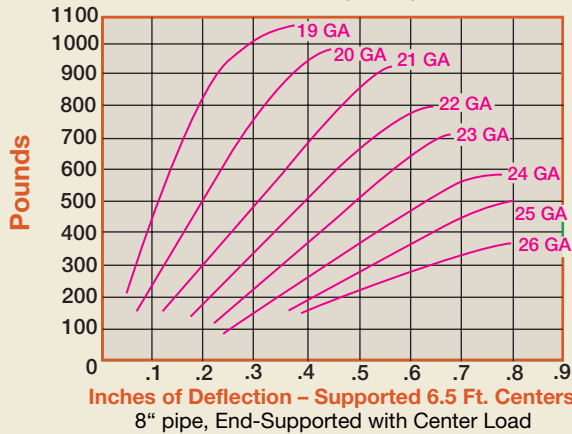
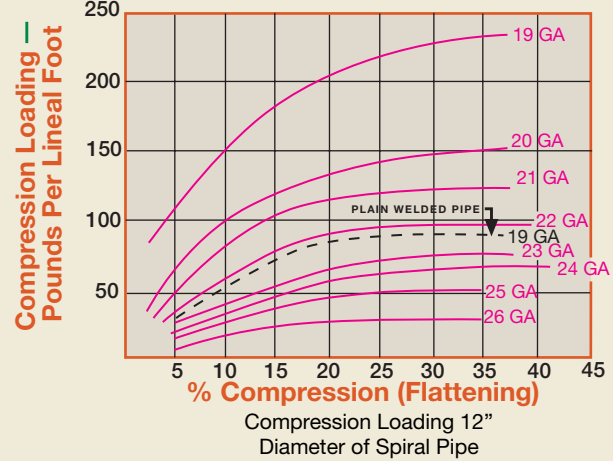
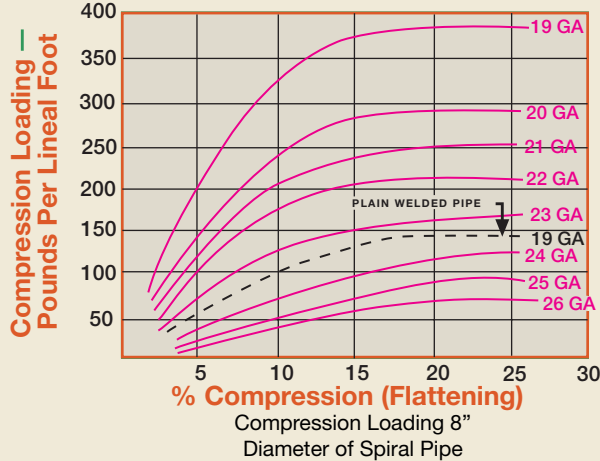
Static Pressure (Friction) Loss of Spiral Pipe



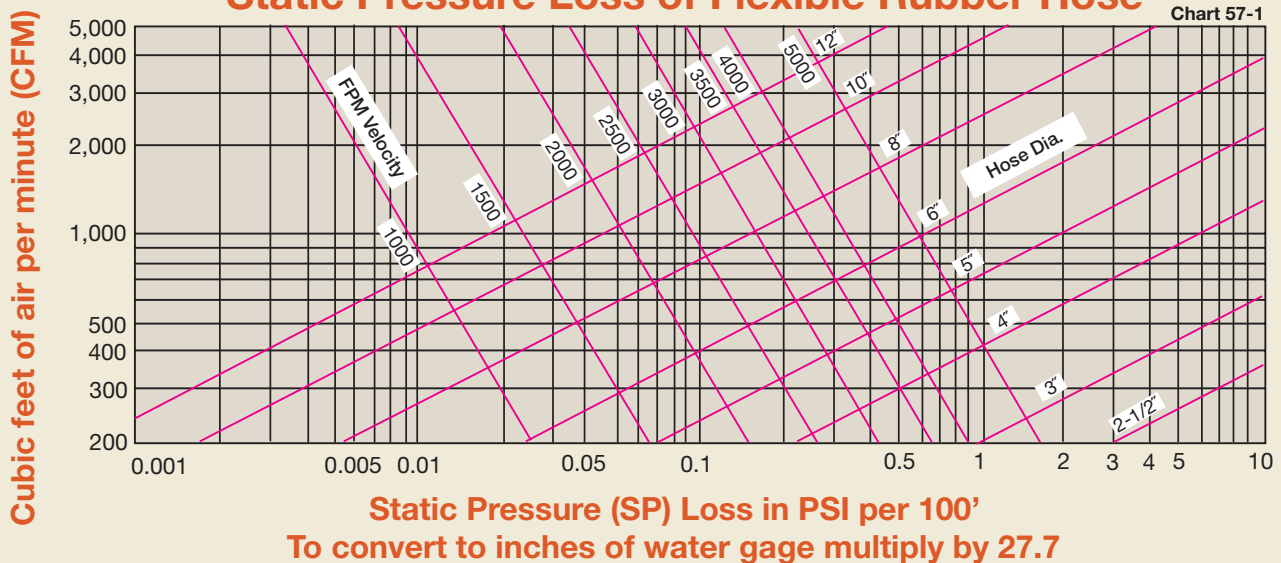
Engineering Data

Compression & Deflection Properties of Spiral Pipe, Static Pressure (SP) Loss in Flexible Rubber Hose

Physical Properties of Spiral Pipe



Static Pressure Loss of Flexible Rubber Hose



Diameter, Gauge & Strength Properties; Collapsing & Bursting Pressures

Engineering Data

Diameters, Gauge, and Strength Properties of Spiral Pipe

Nominal Diameter (inches)	Steel Gauge		Bursting Pressure (Seam Failure) P.S.I		Internal Negative Pressure To Collapse Standard Pipe	
	Std.	Max.	Std.	Max.	In. ~wg	PSI
3	24	22	*	*	**	**
4	24	20	500	*	**	**
5	24	18	350	*	**	**
6	24	18	275	*	**	**
7	24	18	220	*	**	**
8	24	18	175	460	**	**
9	24	18	150	375	304	11.0
10	24	18	135	325	193	7.0
11	24	18	115	275	111	4.0
12	24	18	95	240	83	3.0
13	24	18	85	220	66	2.4
14	24	18	80	185	47	1.7
15	24	18	72	170	44	1.6
16	24	18	65	160	39	1.4
17	24	18	58	145	36	1.3
18	24	18	53	140	35	1.25
20	24	18	47	120	33	1.2
22	24	18	41	100	33	1.2
24	22	18	48	87	33	1.2
26	22	18	42	78	***	***
28	22	18	37	68	***	***
30	22	18	33	60	***	***
32	22	18	30	55	***	***
34	22	18	28	52	***	***
36	22	18	27	48	***	***
42	22	18	29	37	***	***
48	22	18	25	32	***	***

*Did not fail at 500 PSI ** Did not fail at -14.7 PSI (-407 in. H₂O)
*** Less than 1.2 PSI

Calculation of wall thickness to diameter ratio: $(\frac{T}{D})$

Example: For 24 gauge steel and duct diameter of 13".

$$(\frac{T}{D}) = .0296/13 = .0023$$

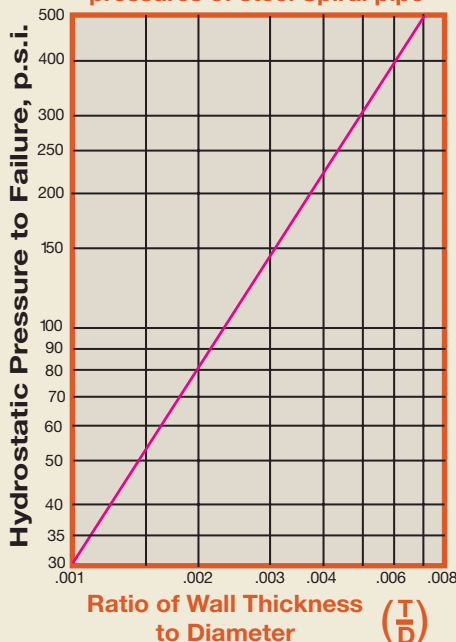
Above reference, for lower charts, to predict bursting and collapsing pressures.

Gauge	Mean Thickness
16	.0635
18	.0516
20	.0396
22	.0336
24	.0276
26	.0217

$$1 \text{ PSI} = 27.7 \text{ ~wg} \quad 1 \text{ ~wg} = .0361 \text{ PSI}$$

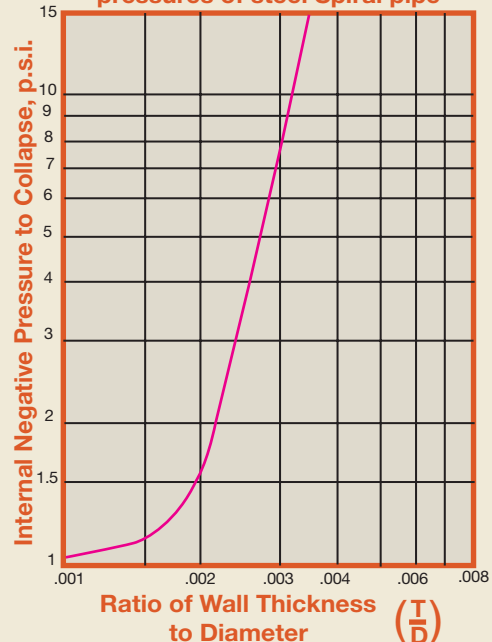
Properties are approximate, based on both empirical and extrapolated data

Chart to predict bursting pressures of steel Spiral pipe



Refer to upper right corner of page for more details

Chart to predict collapsing pressures of steel Spiral pipe



Refer to upper right corner of page for more details

